

Fluid Dynamics and Chemistry in Effective Polymer Mixing for Improved Flocculation

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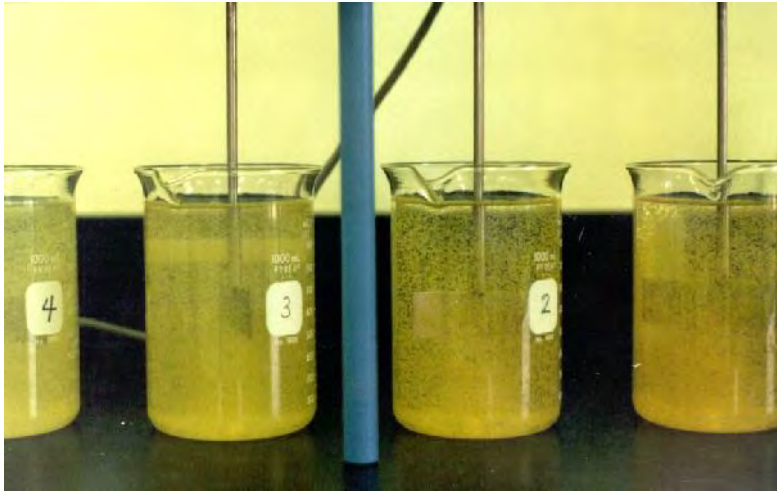


Presentation Overview

- Why Polymer?
- Characteristics of Polymer
- Effect of Dilution Water Chemistry
- Effect of Mixing Energy/Strategy
- Exemplary Polymer Systems

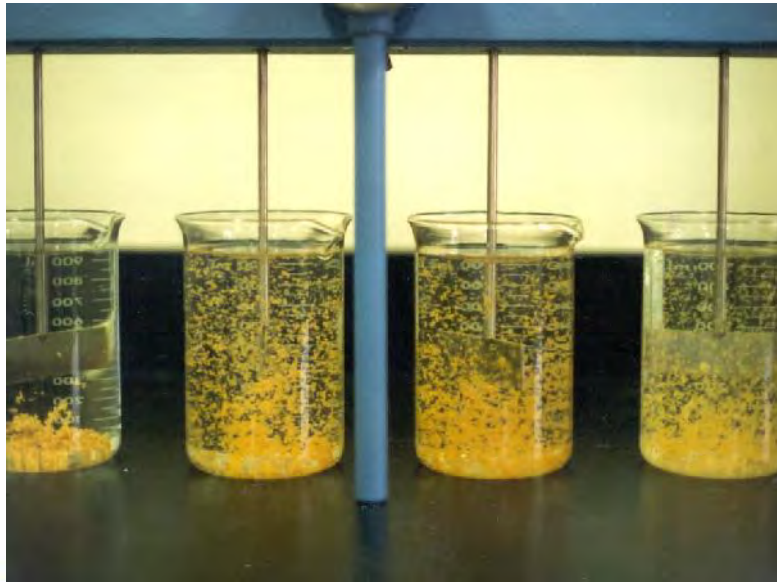


Coagulation and Flocculation



Coagulation

- Double-layer compression (charge neutralization)
- Enmeshment (sweep coagulation)
- Clay suspension + Ferric chloride

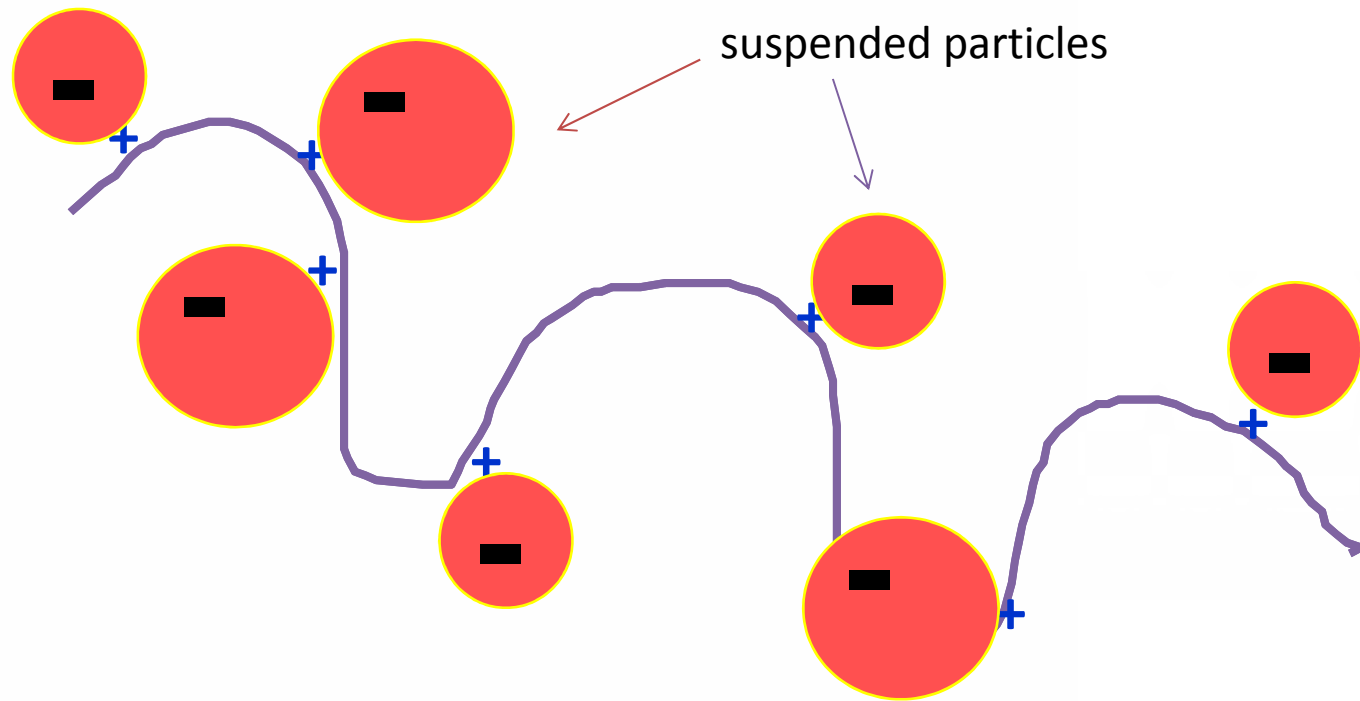


Flocculation

- Polymer Bridging
- Clay suspension + Ferric chloride + Polymer (0.1 - 1 ppm)



Flocculation - Bridging by Polymer Molecules



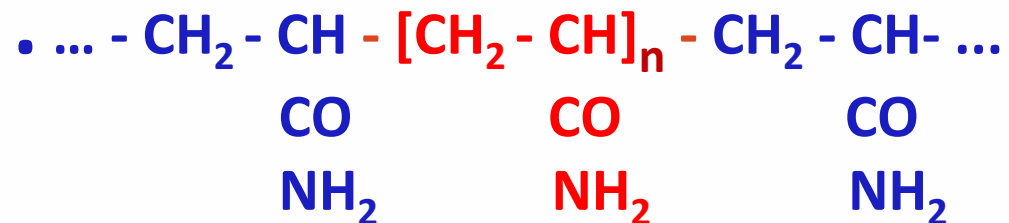
Extended cationic polymer molecule attracts negatively-charged suspended particles

Coagulants and Flocculants

Coagulants (low mol. wt.)	Inorganic	Cationic	Alum, Ferric Chloride Polyaluminum Chloride (PAC)
	Organic	Cationic	PolyDADMAC Epi./DMA
Flocculants (high mol. wt.)	Organic	Cationic	Acrylamide/amine copolymer Mannich polymer
		Anionic	Acrylamide/acrylate copolymer
		Nonionic	Polyacrylamide Polyethylene oxide

Structure of Polymer

- Polymer Flocculant, Linear Polymer, Polyelectrolyte
- Chained Structure by Repetition of Monomers



Most polymers in water industry are acrylamide-based.

If molecular weight of polymer is 10 million,
the number of monomers in one polymer molecule, “*degree of polymerization*”

$$\begin{aligned} n &= 10,000,000 / 71 \\ &= 140,850 \end{aligned}$$

(mol. wt. of monomer, acrylamide = 71)



High Molecular Weight Polymers

Dry Polymer

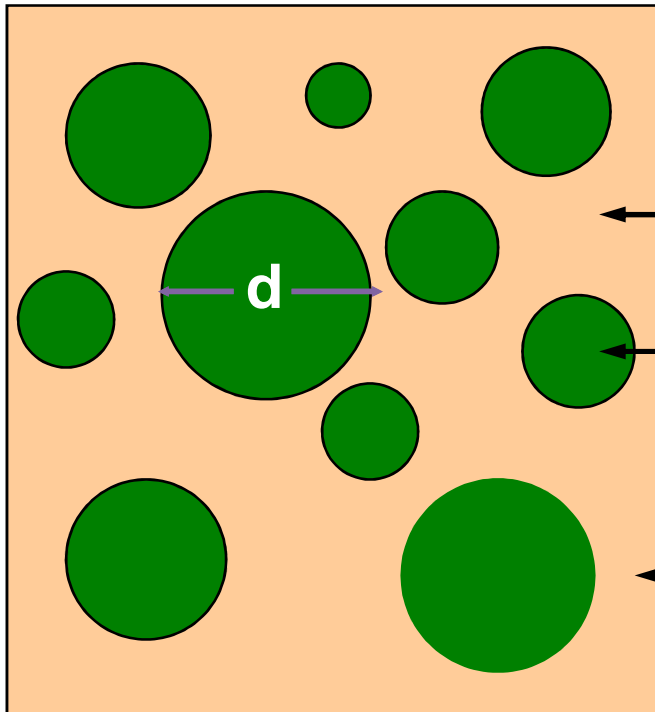
- Cationic, anionic, non-ionic
- Molecular weight: up to 10 M (cationic), up to 20 M (anionic, non-ionic)
- > 95% active
- Polymer particle size: 0.1 to 1 mm
- Cost: high

Emulsion Polymer

- Cationic, anionic, non-ionic
- Molecular weight: up to 10 M (cationic), up to 20 M (anionic, non-ionic)
- 30 - 60% active
- Polymer gel size: 0.1 to 2 μm
- Cost: very high



Emulsion Polymer - 40% active



Hydrocarbon Oil: 30%

Polymer Gel: Polymer 40%
Water 30%

- Stabilizing surfactant
- Inverting (breaker) surfactant

To maximize the value of Inverting Surfactant*

* Higher polymer concentration first (1%)

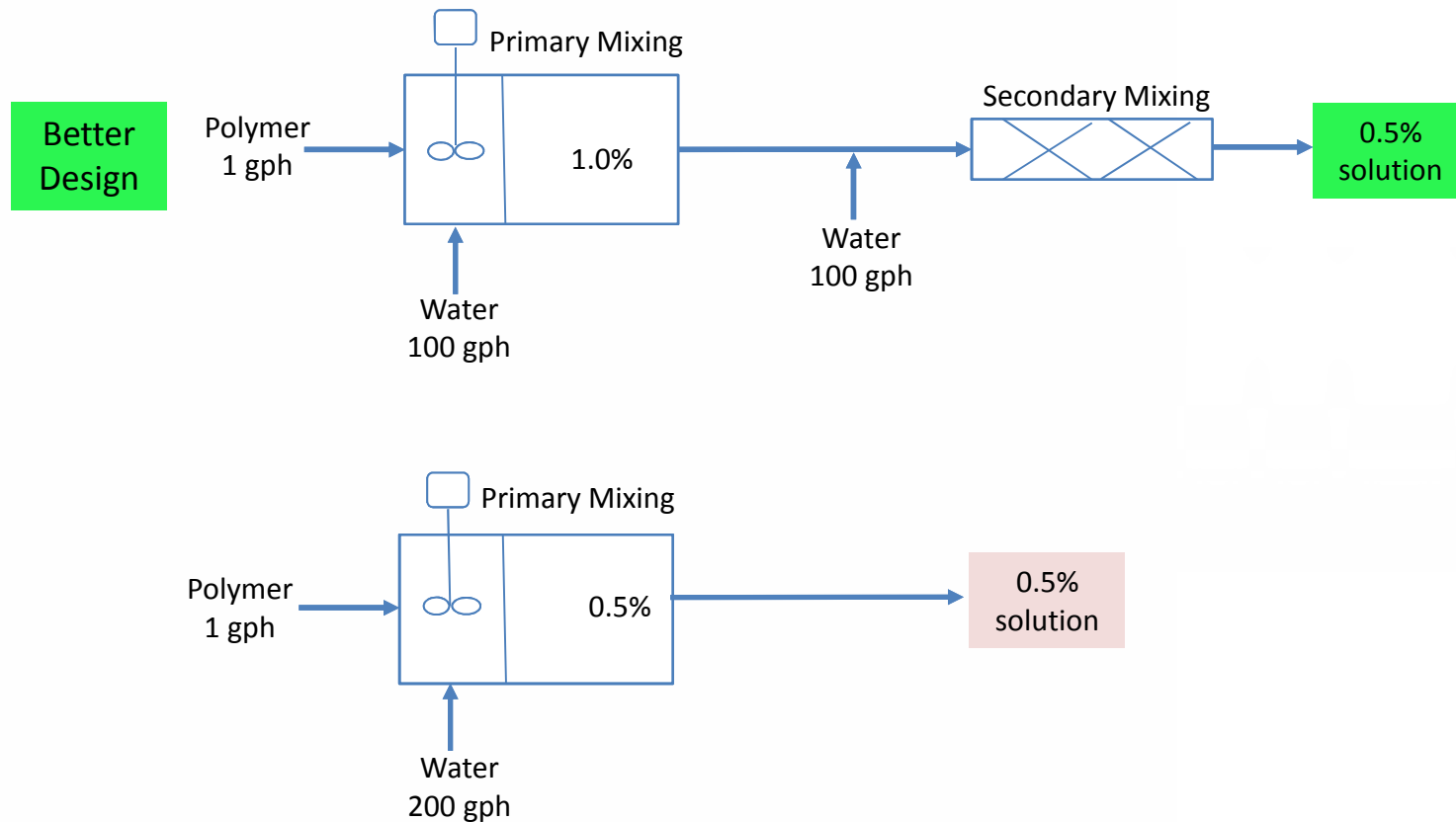
* Post-dilution to feed concentration (0.5%, 0.25%)

$d = 0.1$ to $2 \mu\text{m}$

* AWWA Standard for Polyacrylamide (ANSI-AWWA B453-96), 10 - 11, 1996

How to Maximize the Value of Inverting Surfactant?

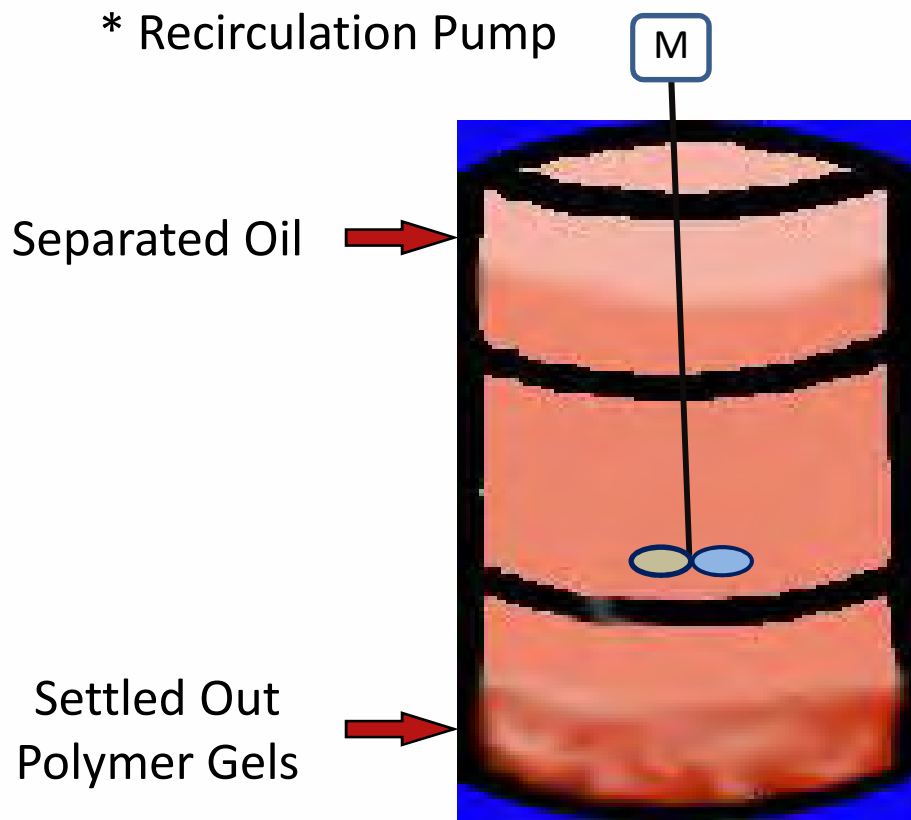
Primary mixing at high % + Secondary mixing at feed %



Storage of Emulsion Polymer

- Separation (stratification)

- * Drum (Tote) Mixer
- * Recirculation Pump



- Moisture Intrusion

- * Drum (Tank) Dryer



Recommended Dilution Water Quality

Ionic strength (Hardness): multi-valent ions; adverse effect

- Soft water helps polymer molecules fully-extend faster
- Hardness over 400 ppm may need softener

Oxidizer (chlorine): detrimental to polymer chains

- Maintain less than 3 ppm

Temperature: higher temperature, better polymer activation

- In-line water heater for water lower than 40 °F
- Water over 100 °F may damage polymer chains

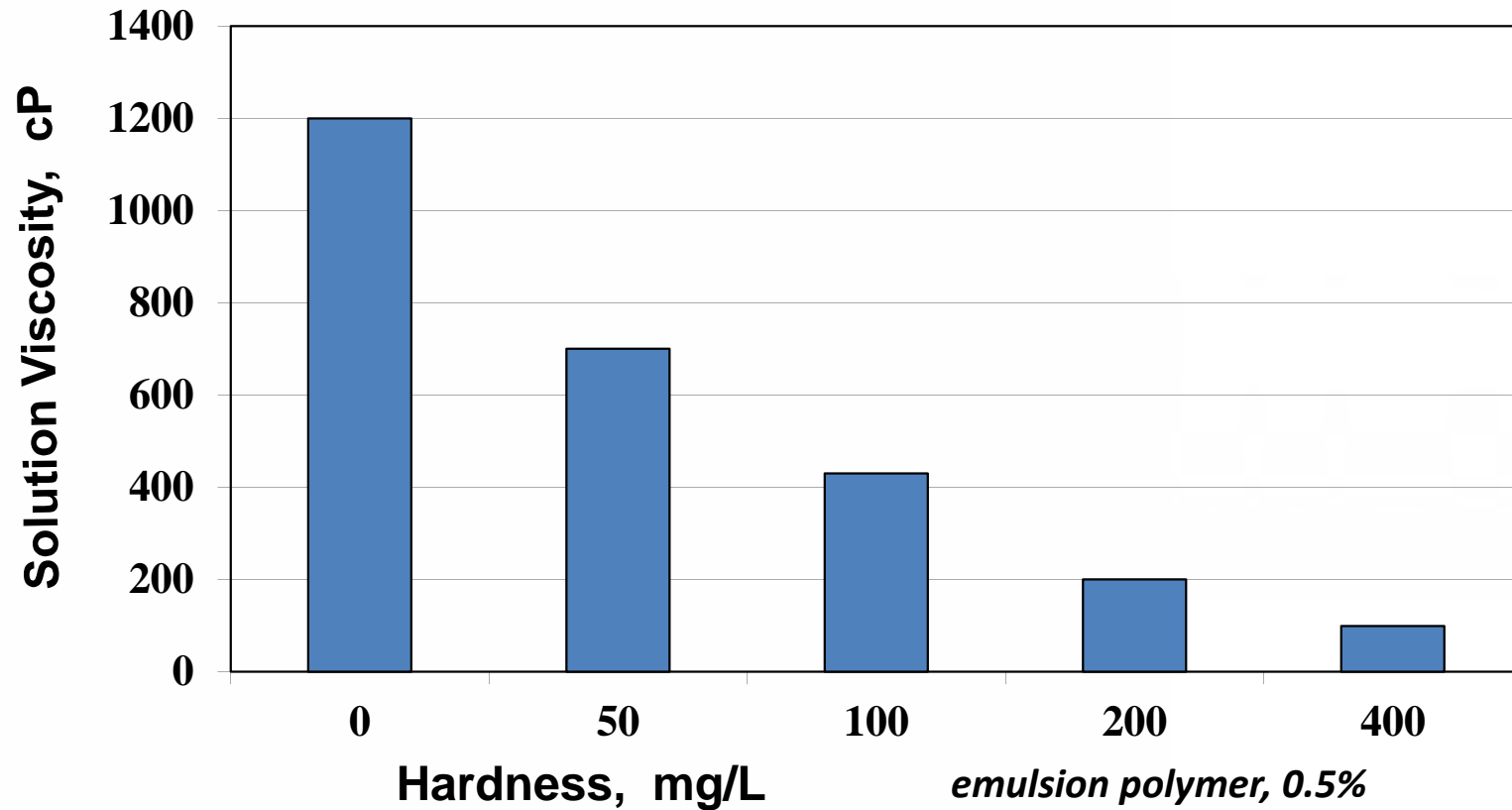
Suspended solids: strainer recommended if > 10 ppm

pH: negligible effect within pH 3 - 10



Effect of Dilution Water Hardness

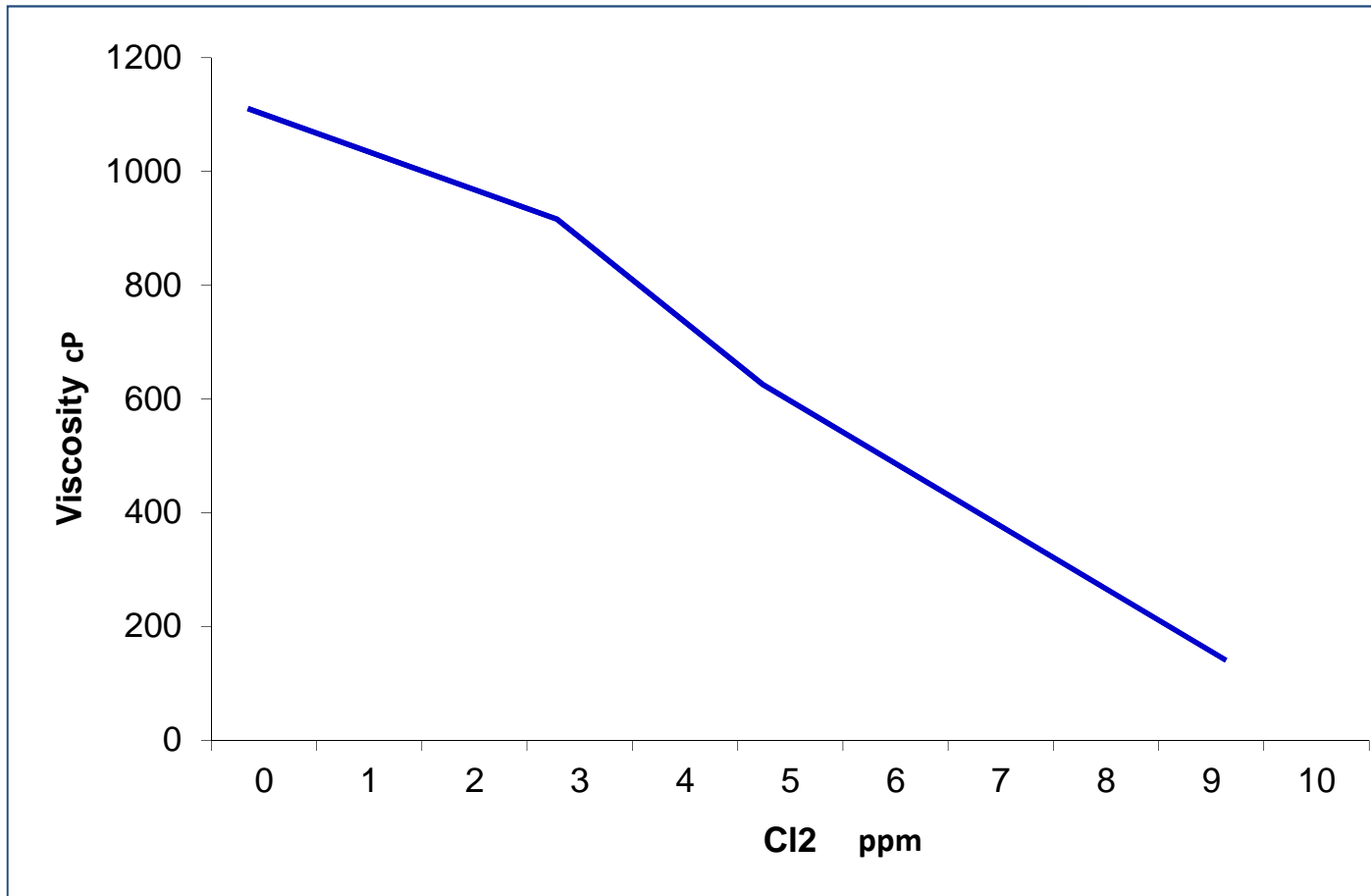
Soft water helps polymer chains to be fully extended



Kim, Y.H., *Coagulants and Flocculants: Theory and Practice*, 43, Tall Oak Pub. Co. (1995)

Effect of Chlorine (Oxidizing Chemical)

Oxidizing chemicals break down polymer chains



Polymer Activation (Dissolution)

1. Initial Wetting (Inversion)

Sticky layer formed

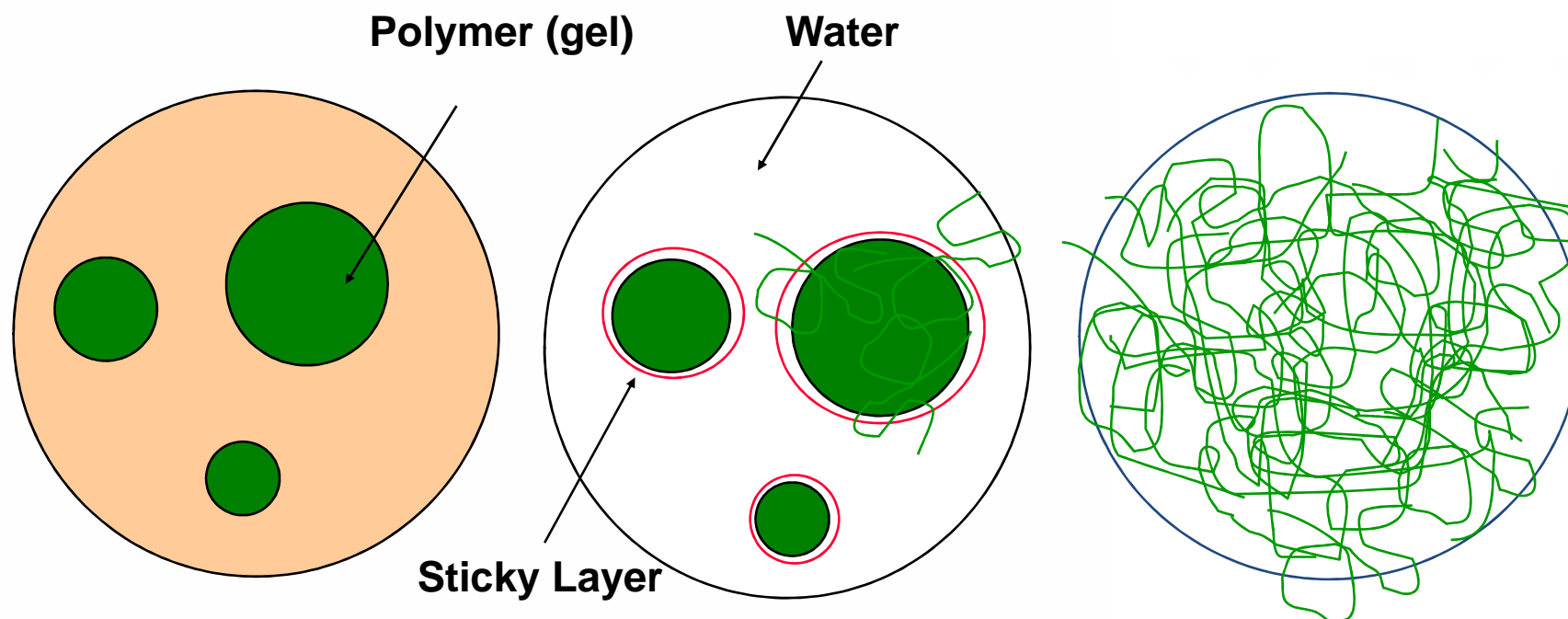
High-energy Mixing Required

2. Dissolution

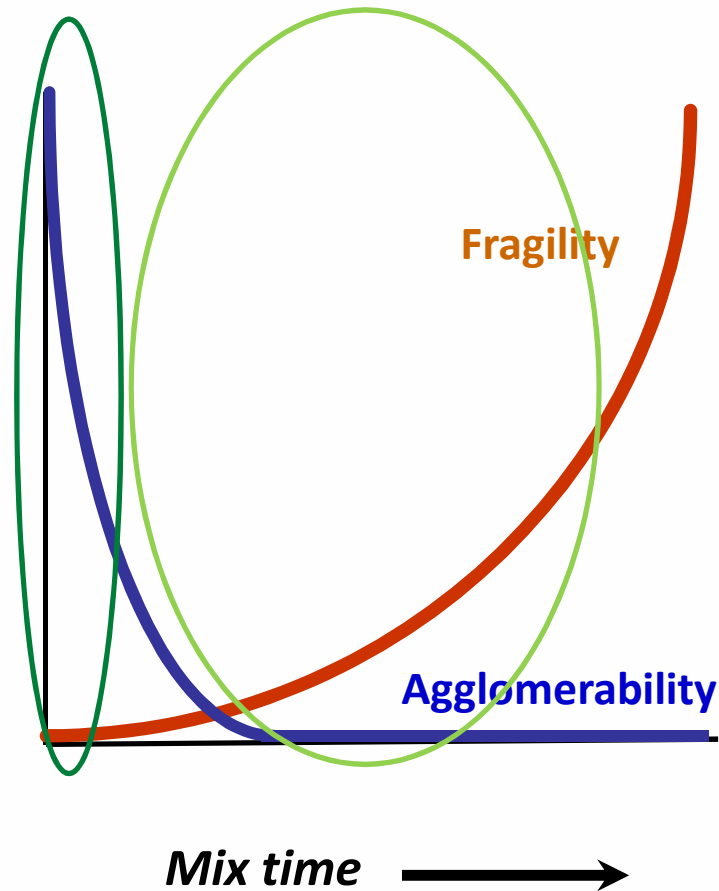
“Reptation” by *de Gennes (1971)**

Low-energy Mixing Required

* de Gennes, P.G., *J. Chem. Phys.*, 55, 572 (1971)



Characteristics of Polymer Activation



Initial wetting stage:

- negligible fragility
- very high-energy mixing
- minimize fisheye formation

Dissolution stage:

- negligible agglomerability
- low-energy mixing
- minimize polymer fracture



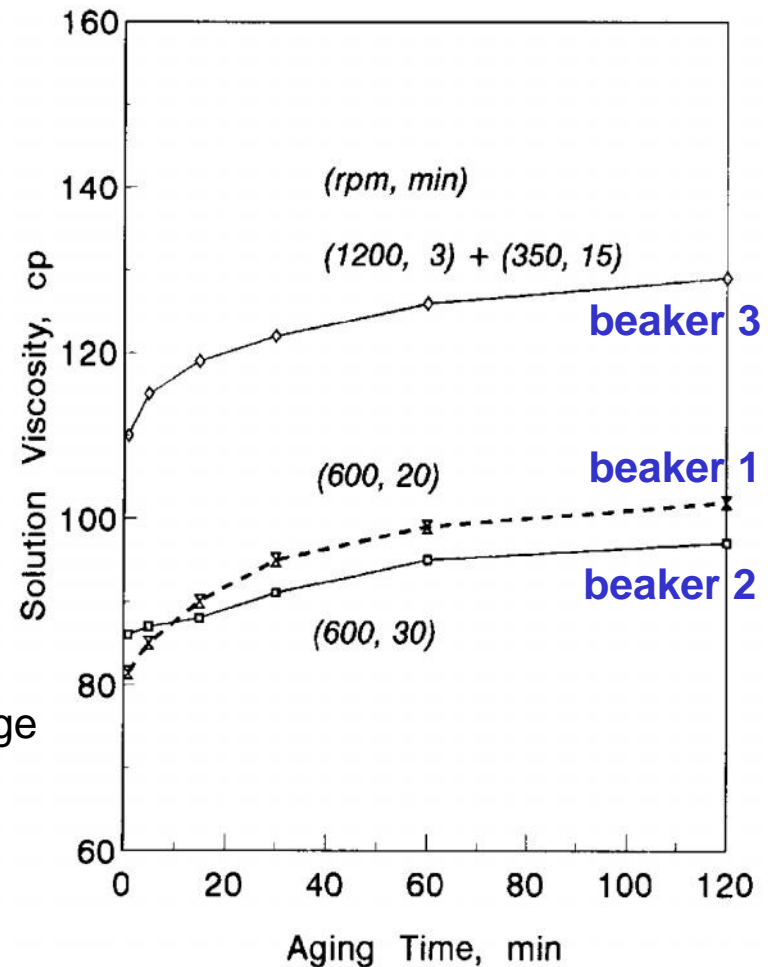
Mixing Effect on Polymer Activation

Viscosity of polymer solution
(prepared in 600 mL beakers)

- Beakers 1, 2: one-stage mixing
- Beaker 3: two-stage mixing

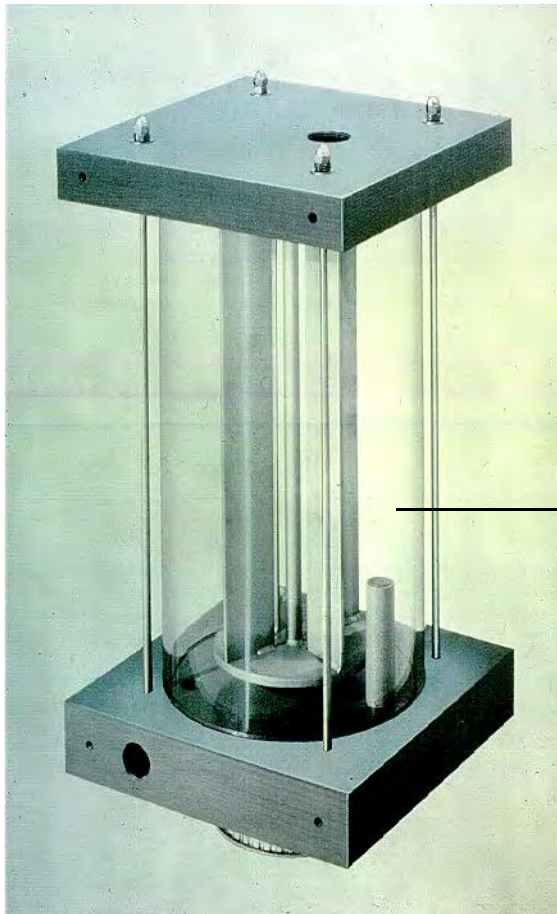
Two-stage mixing resulted in polymer solution of much better quality

- * High energy first: prevent fisheye formation
- * Low energy followed: minimize polymer damage



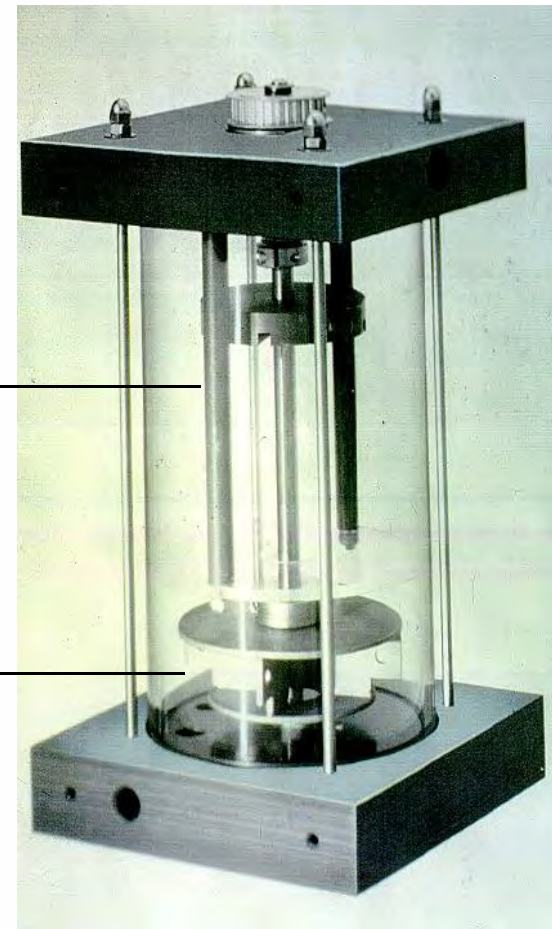
Development of Two-stage Mixer

1- stage mixer



1,700

2- stage mixer



1,100

4,000

G-value, mean shear rate (sec^{-1})

Mixing Effect on Polymer Activation

Two-stage mixing → significant increase in polymer solution viscosity

Polymer	Mixing unit	Conc. %	Viscosity cP
Anionic	1-stage	0.50	226
	2-stage		310 (27%↑)
Cationic	1-stage	0.50	427
	2-stage		523 (18%↑)
Nonionic	1-stage	0.50	156
	2-stage		178 (12%↑)

PolyBlend[®] PB Series

- The Original PolyBlend[®] System
- Proven performance
- Two-Stage mixing
- Rugged
- Economical
- Portable
- Space saving
- Optional A-control
- Ship next day



PolyBlend[®] M Series

- Open-Frame Design
- Easy Installation & Maintenance
- Direct Drive Mixing
- Variable Speed Mixing
- Choice of Polymer Pumps
- On-board Post-dilution
- Optional Custom Controls*
A, B, C Control



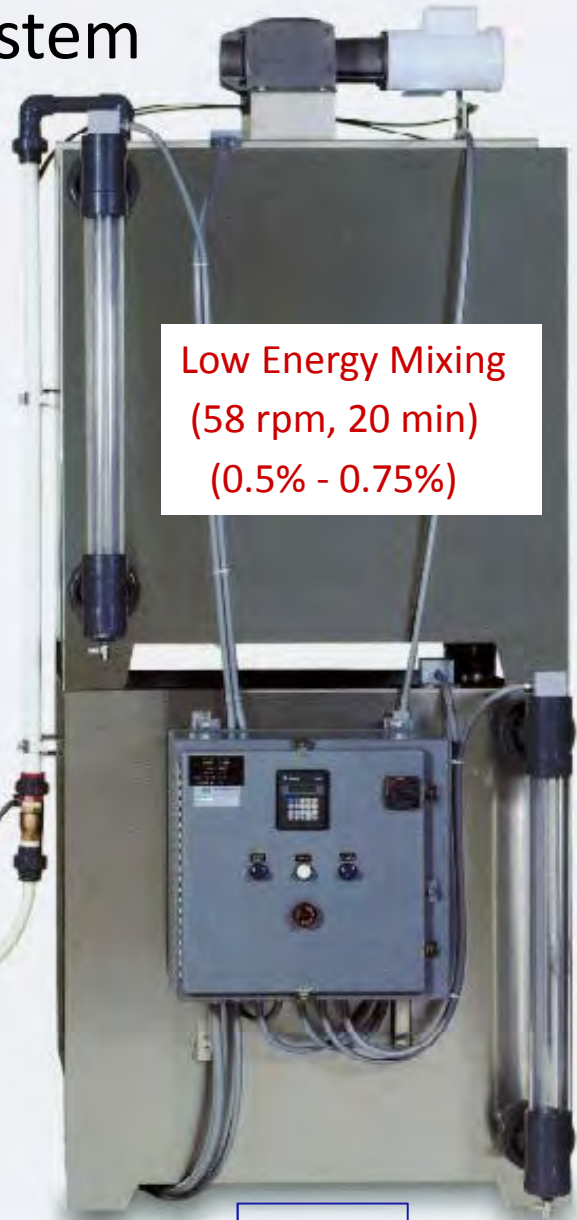
PolyBlend Dry Polymer System

High Energy Mixing
 $G = 15,000 / \text{sec}$
(3,450 rpm, <0.5 sec)



DD4

Low Energy Mixing
(58 rpm, 20 min)
(0.5% - 0.75%)



DP800

Post-dilution
(0.1% - 0.2%)



Final Feed Skid

Dry Disperser (DD4) for Initial Wetting

Very High-Intensity Mixing for Short Time

$G = 15,000$ /sec

@ 3,450 rpm

for < 0.5 sec

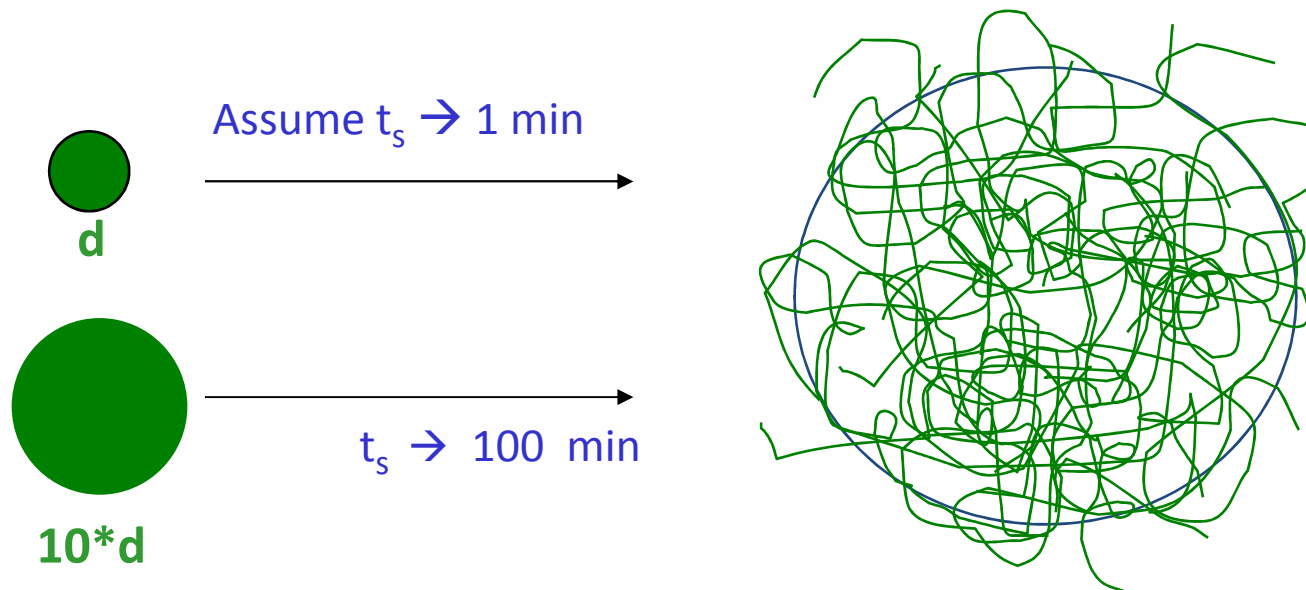
Disperses Individual Polymer Particles

- * No Fisheye Formation
- * Shorter Mixing Time in Next Stage



Why initial high-energy mixing is critical?

Polymer swelling time, $t_s = k (\text{diameter})^2$ *Tanaka (1979)**



Initial high-energy mixing (DD4) \rightarrow No fisheye formation \rightarrow Significantly shorter mixing time \rightarrow Minimum damage to polymer structure \rightarrow Better quality polymer solution \rightarrow Less polymer consumption

* Tanaka, T., Fillmore, D.J., *J. Chem. Phys.*, 70 (3), 1214 (1979)

Mixing Tank for Dissolution of Dry Polymer

Patented Hollow-Wing Impeller

- No Weissenberg Effect

Large Impeller, $d/D > 0.7$

- Uniform Mixing Energy

Low RPM, 60 - 115 rpm

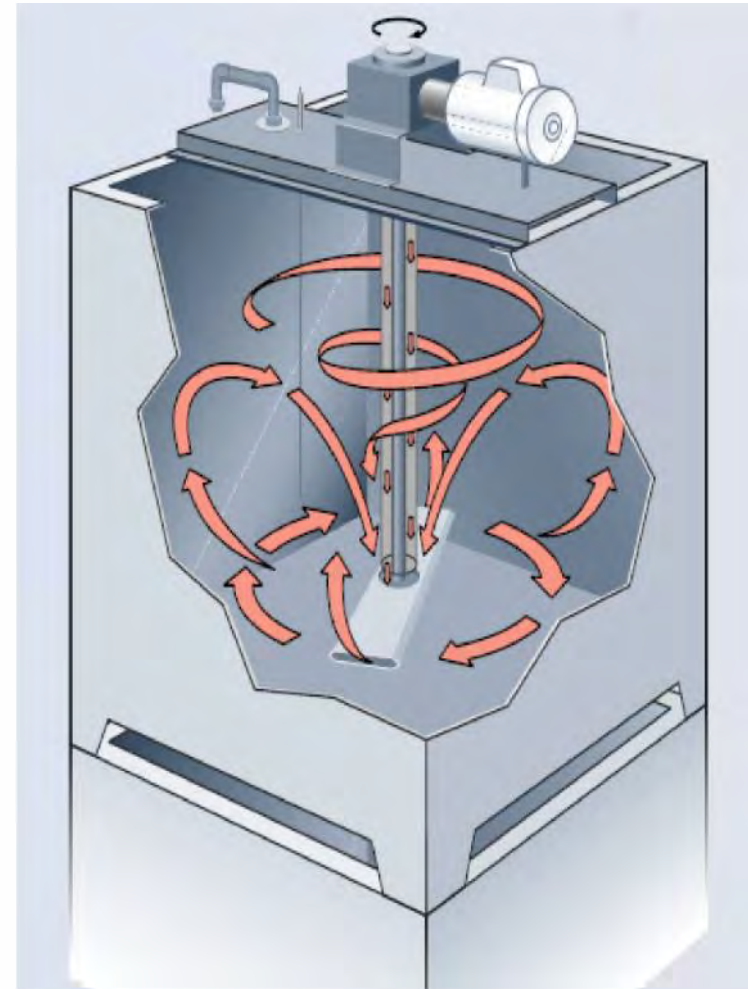
- Low-intensity Mixing
- Minimize Damage to Polymer Chain

Square Tank Design

- No Weissenberg Effect
- No Baffles Needed, No Dead Zone

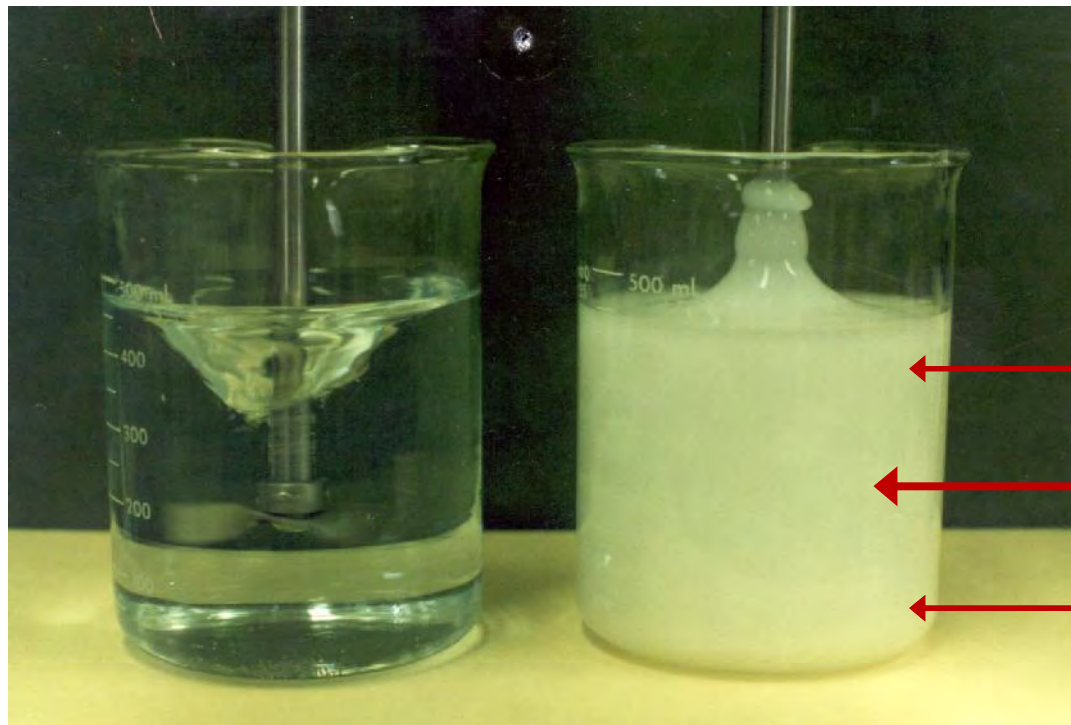
Shorter Mixing Time – Due to DD4

- 20 Minutes for Cationic Polymer
- 30 Minutes for Anionic Polymer
- Minimize Damage to Polymer Chain



Weissenberg Effect

- * Polymer solution exceeding “critical concentration” climbs up mixing shaft
- * Extremely non-uniform mixing
- * Critical factor in designing polymer mix tank - 0.25% limit for HMW polymer



← extremely low mixing

← very high mixing

← extremely low mixing

Water
(Newtonian)

Polymer Solution
(Non-Newtonian, Pseudoplastic)



Thank You

Please contact Yong Kim with any questions

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